

Reliable Electricity Based on Electrochemical Systems (REBELS)

Lower Cost Devices with New Functionality

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Advanced Research Projects Agency - Energy

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Outline

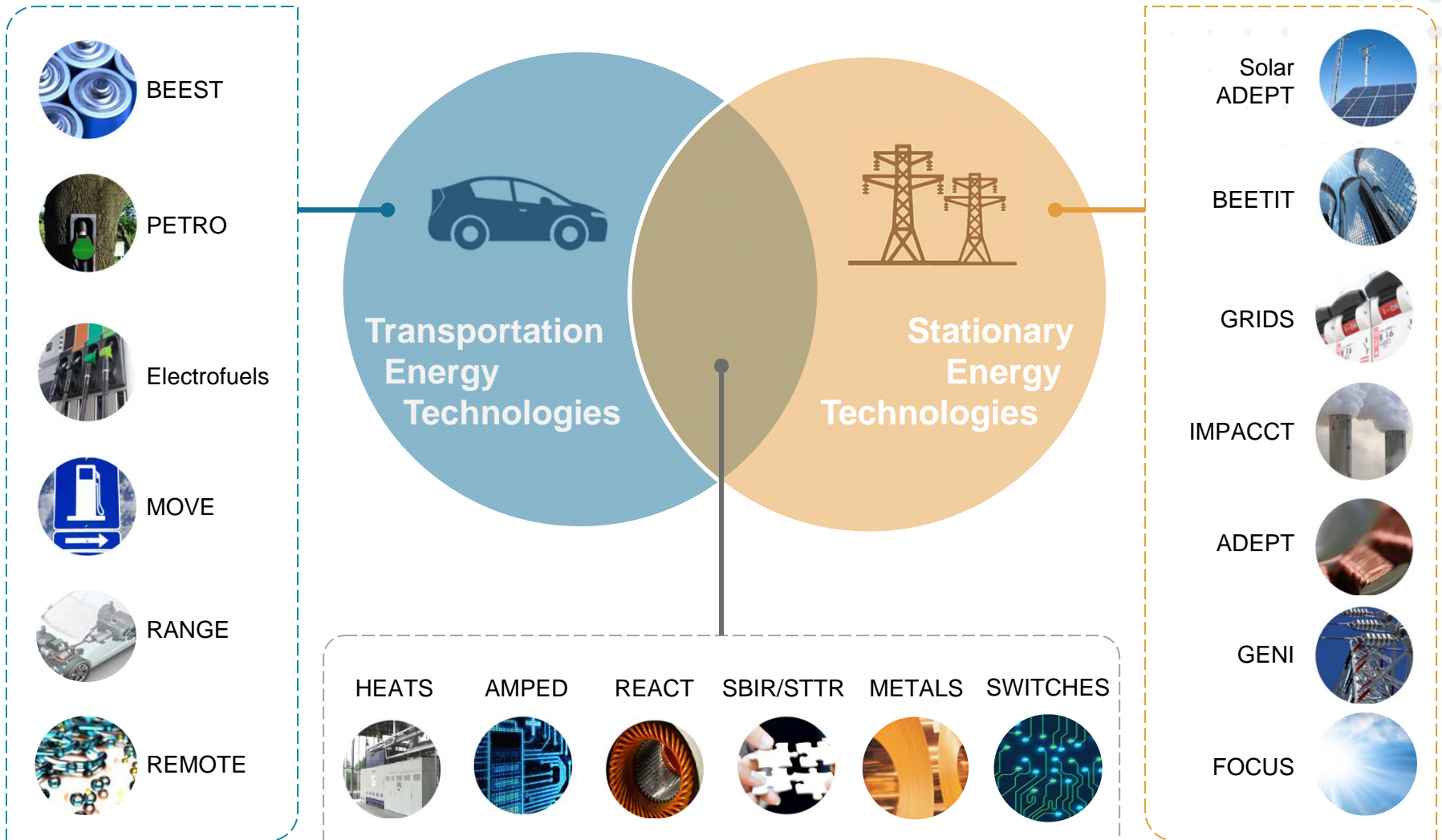
Context Behind REBELS

- Materials
- Distributed Generation Applications

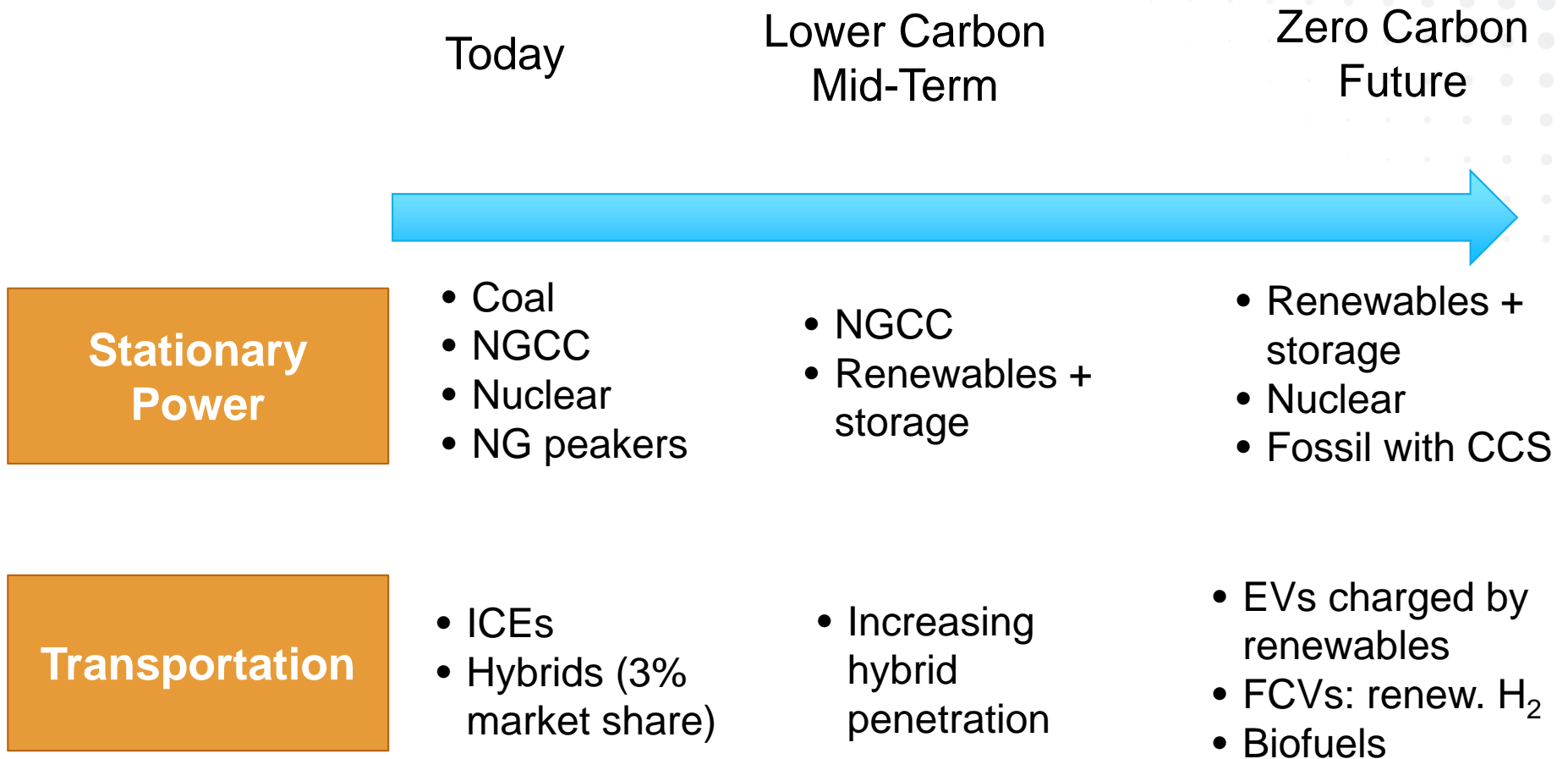
Technical Categories and Project Examples

Summary

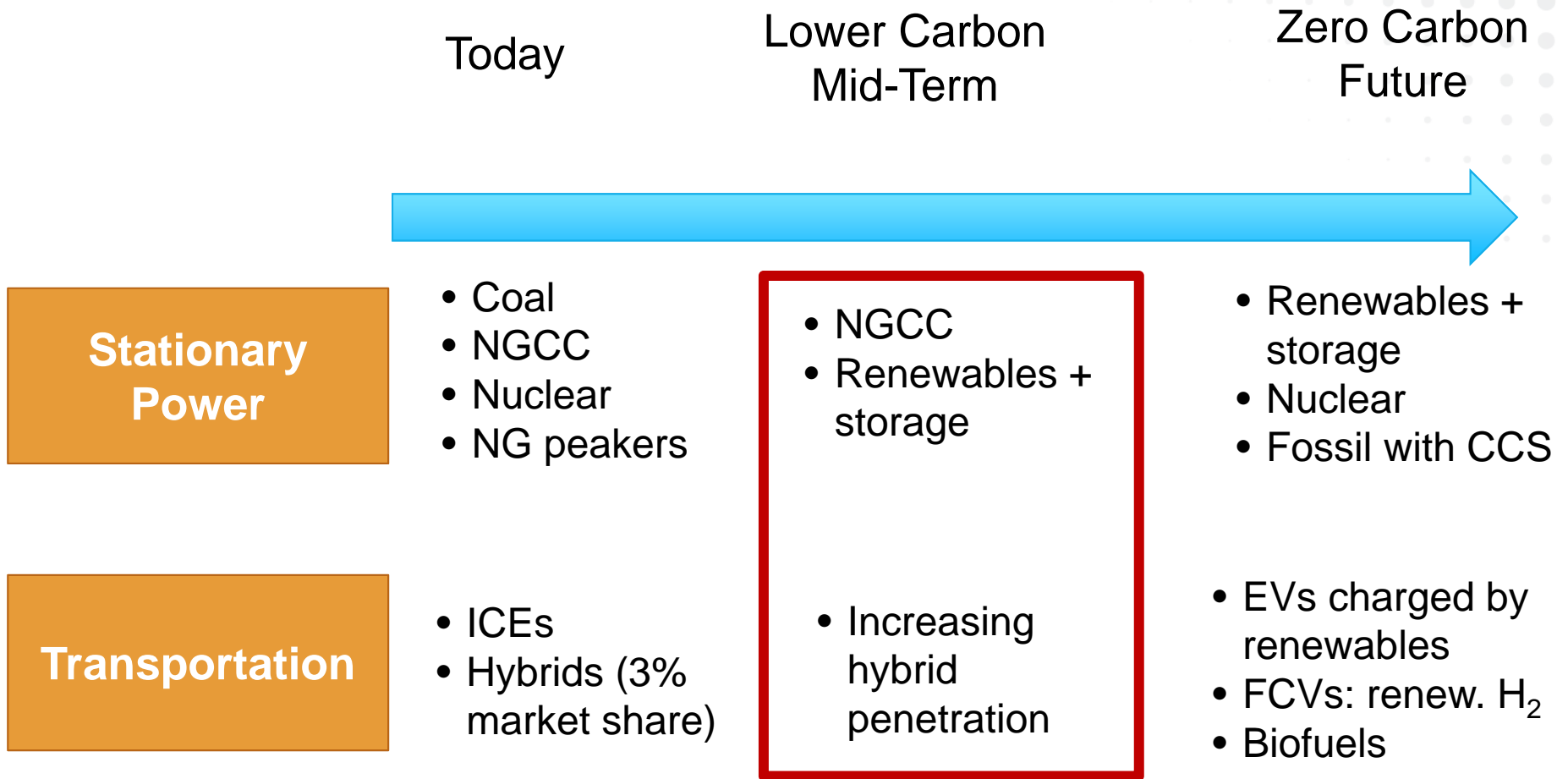
Focused Programs



Bridge to Nowhere the Future



Bridge to Nowhere the Future



Problem: anything 'better' than NGCC or hybrid vehicles costs too much

Stationary Power Today



Strengths

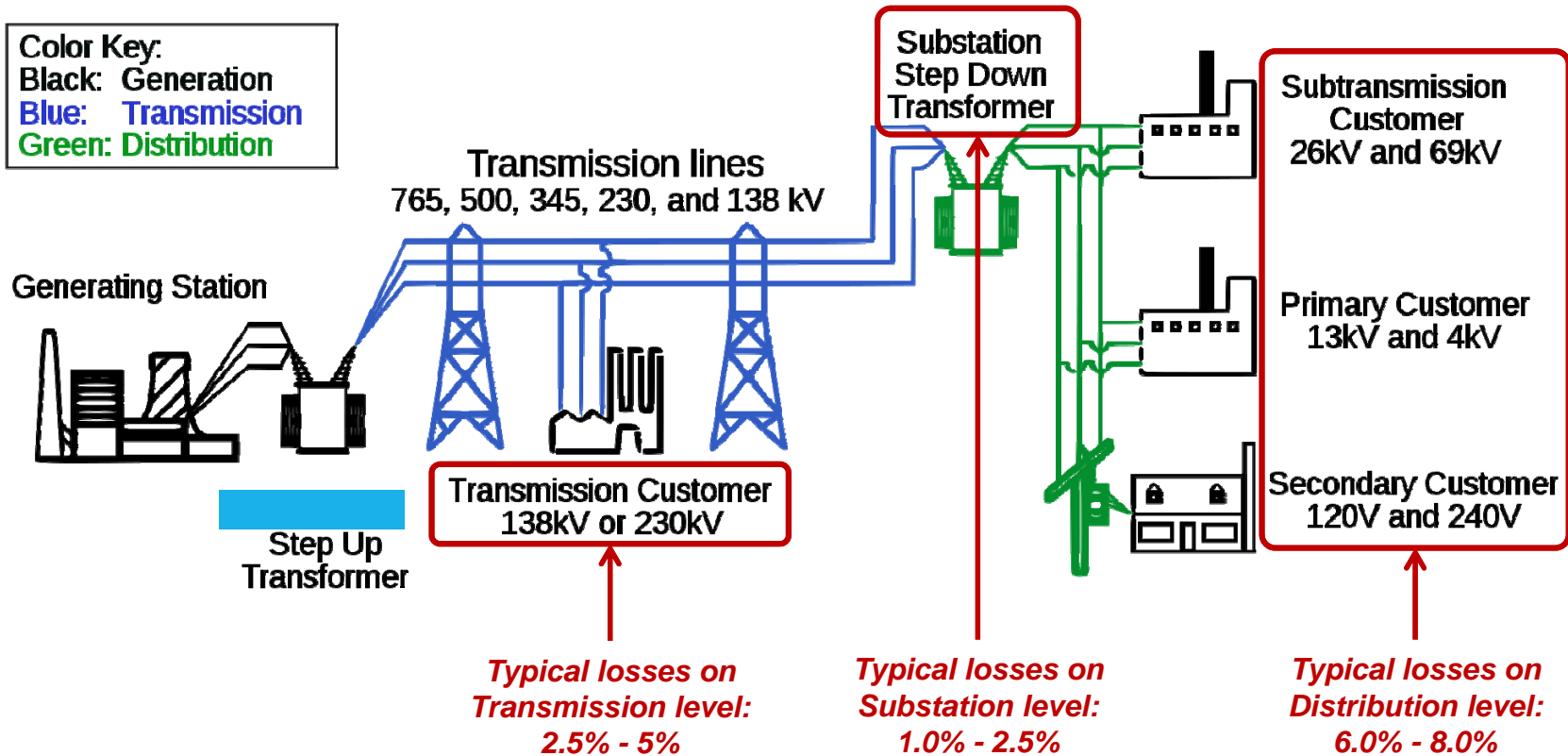
- ~55% efficiency (HHV) for NGCC
- CO₂ point source for future CCS
- High capacity factor
- Mature technology

Weaknesses

- T&D Losses
- Grid vulnerability to natural disasters and terrorist attacks
- Difficulty in integrating intermittent renewable technologies
- Future efficiency gains incremental

Future generation dominated by NGCC and increasing renewables

Energy Loss in Today's Grid



Note: The losses above are at peak load, based from a study of AEP's T&D system. The ranges above do not directly correlate to the previous page due to differences in source data

The majority of the losses are in the distribution level

N2

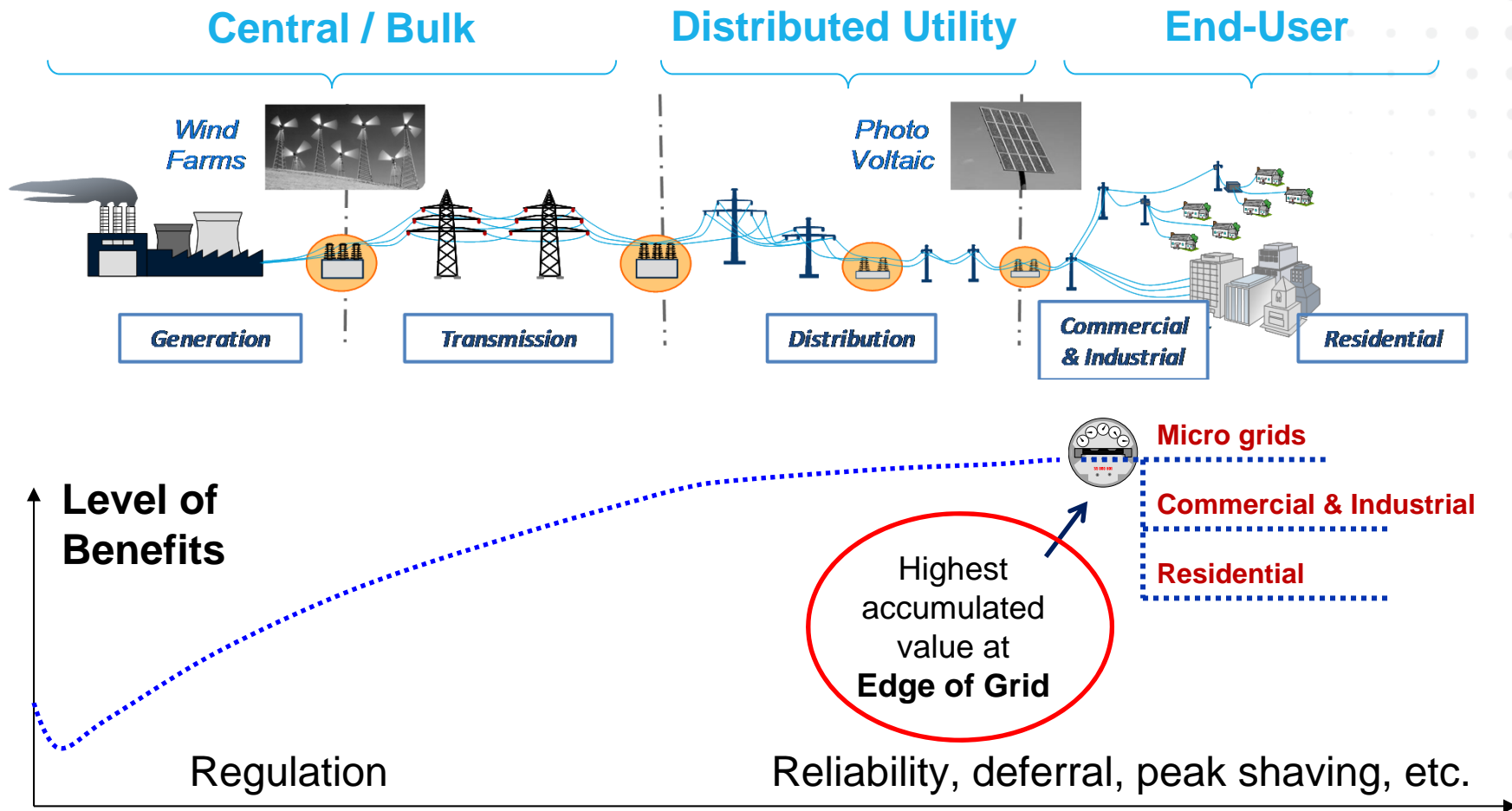
Slide 7

N2

This is something I would emphasize in your voice track. I suggest simply leaving the graphic and speaking to it-losses at different levels.

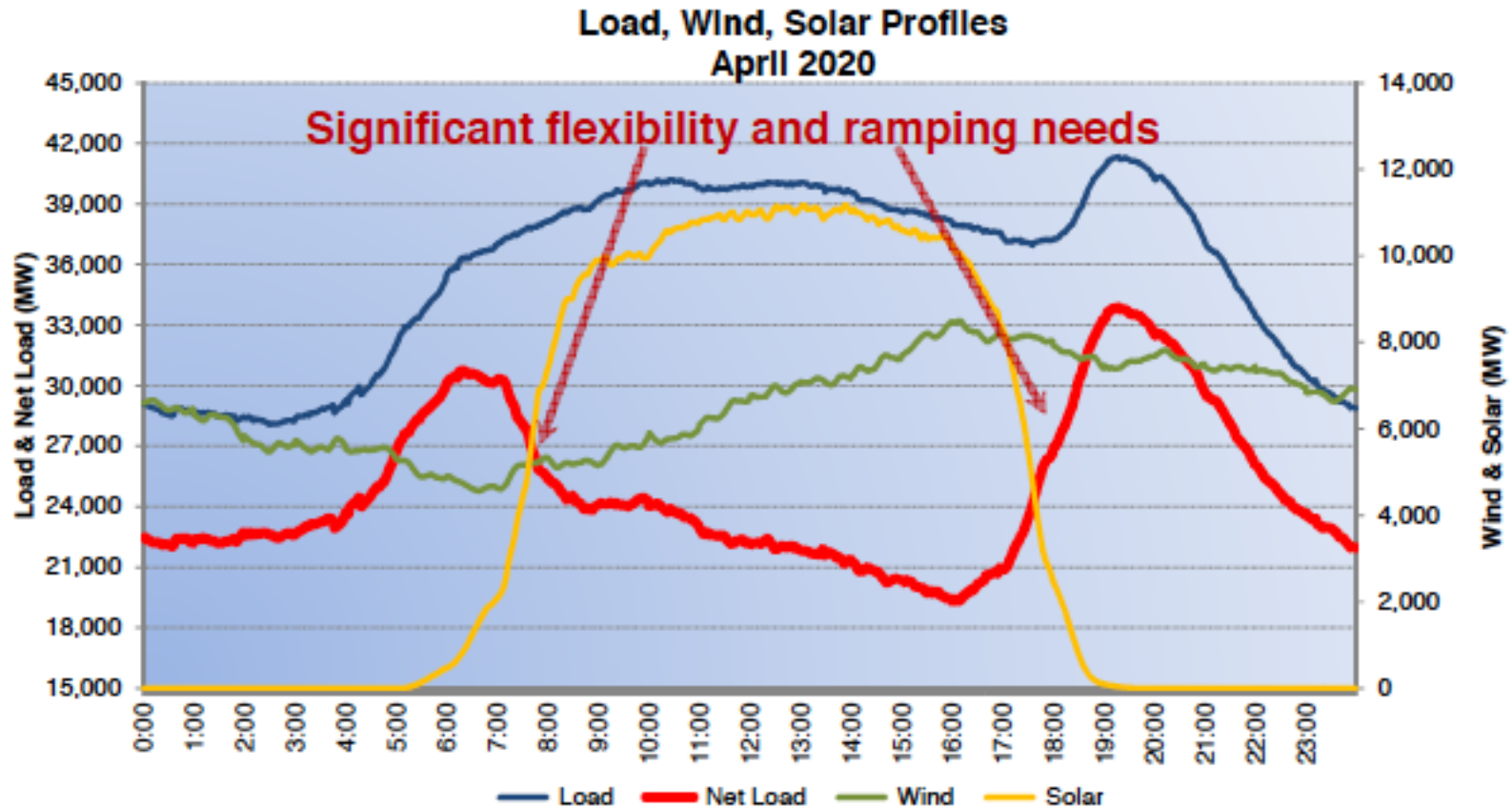
Nikki.Cope, 2/10/2014

The Value of Distributed Generation (DG)



Early movers: Verizon, Microsoft, Google, Big Box Stores, etc.

Impact of PV, Wind on Baseload



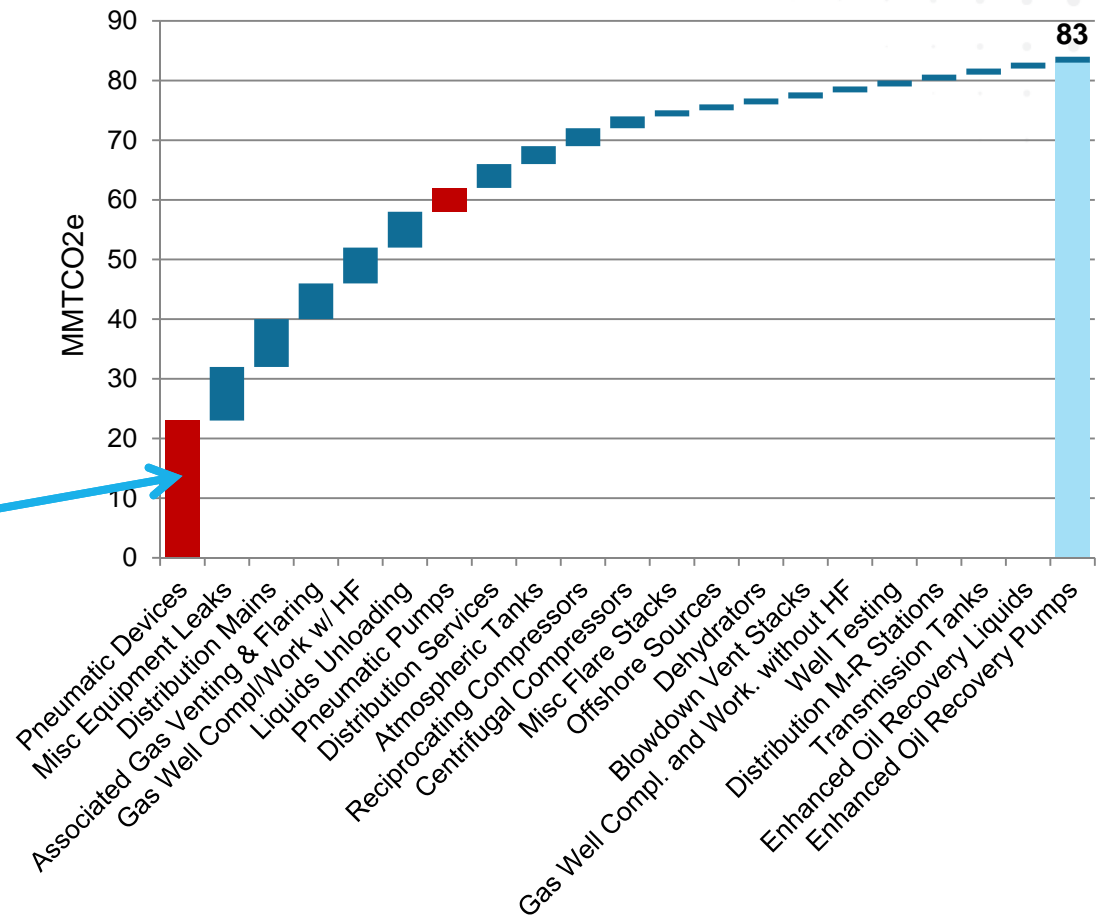
Decrease in base load requires significant reserves to offset high ramps

Small DG Opportunity: Remote NG Wellpads

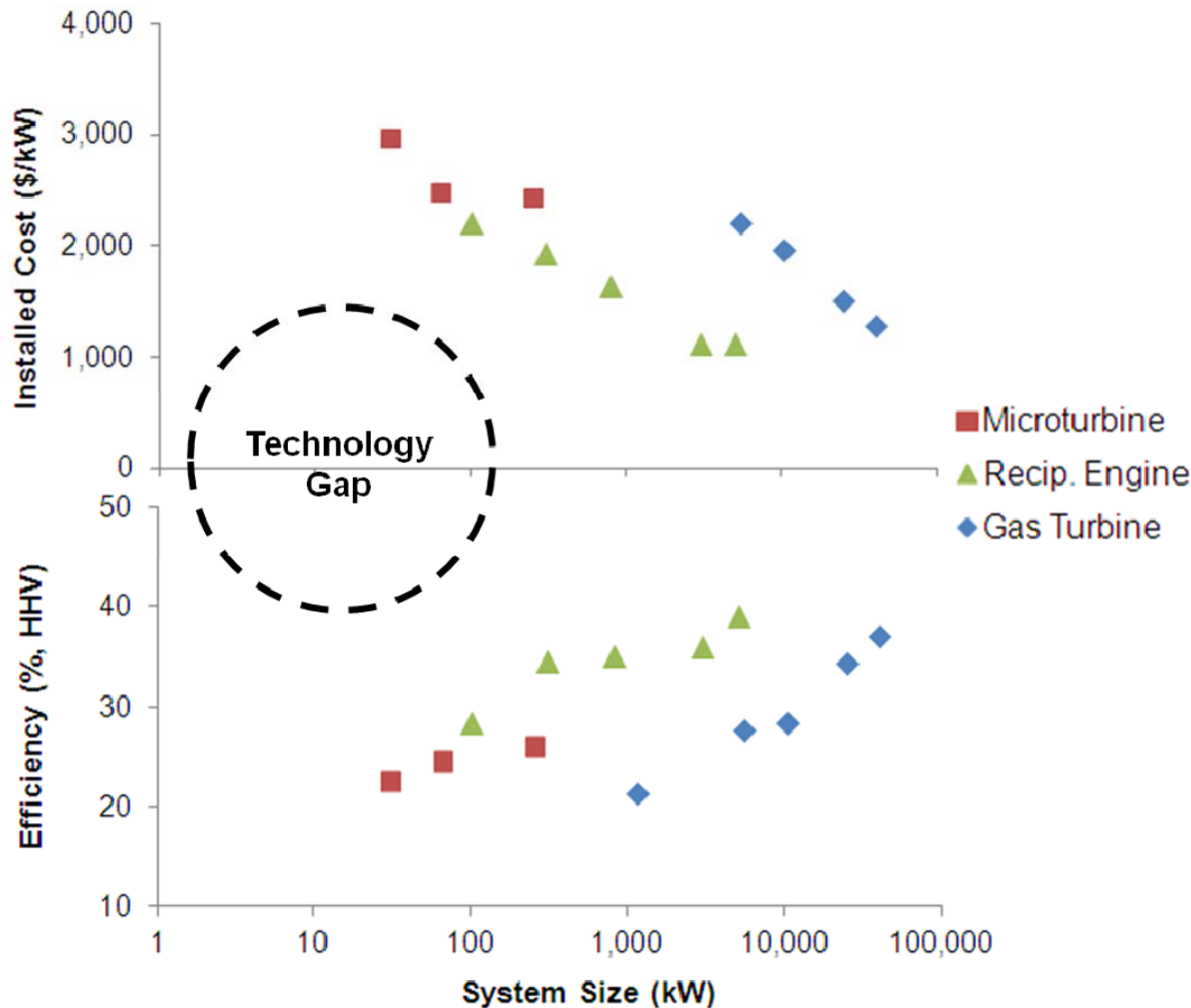
Pneumatic devices use NG pressure to drive pumps, regulators, and valves & then vent it

Results in 20%-35% of methane emissions from the NG production sector

Methane Emissions from Natural Gas Process Sources (2011)

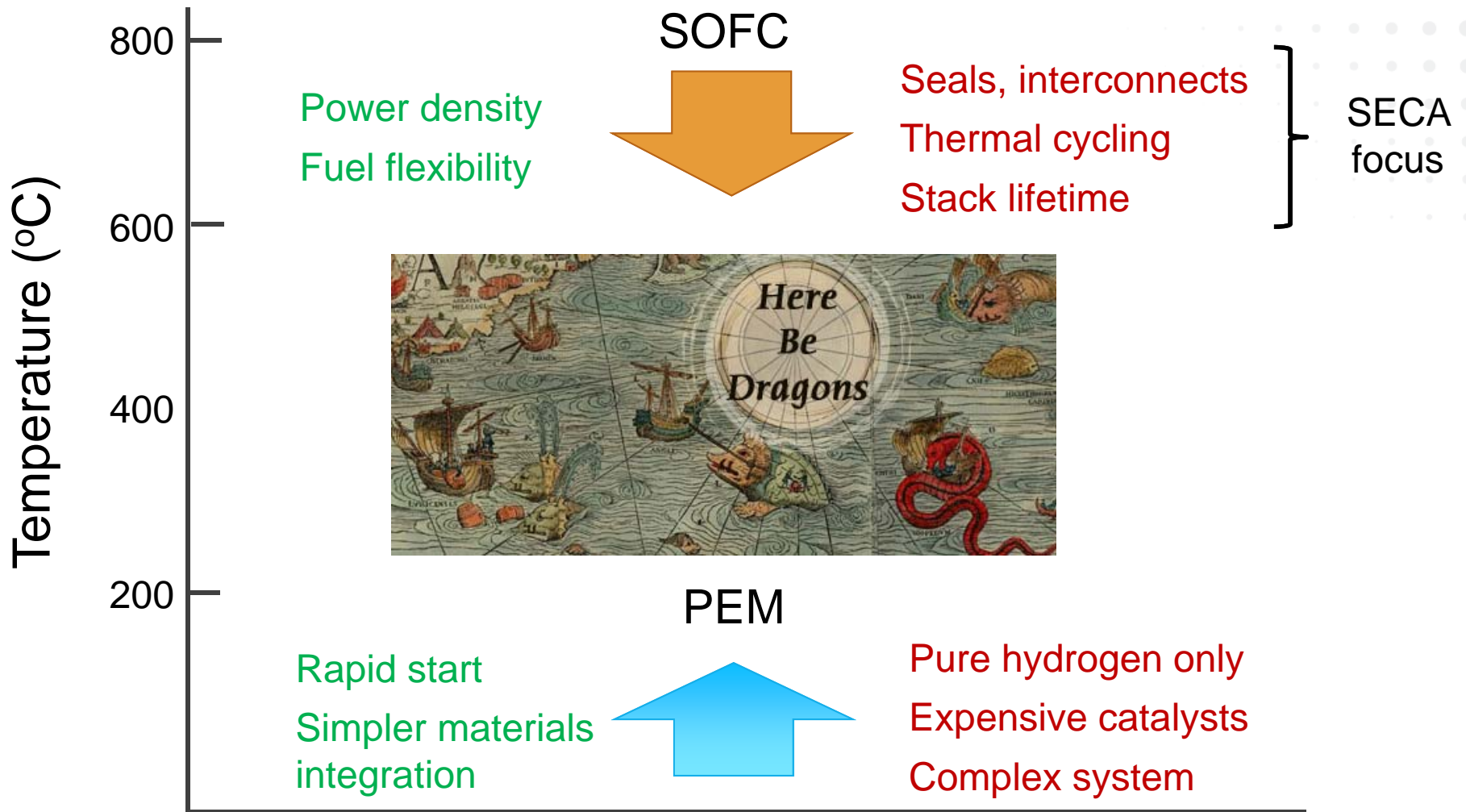


Small DG Prime Movers



Maintenance Intervals (hrs)	
Gas Turbine	4,000-8,000
Microturbine	5,000-8,000
Recip. Engine	1,000-2,000
Fuel Cells	20,000 – 40,000+

Existing Fuel Cell Research Thrusts



Intermediate Temperature Fuel Cells (ITFCs)

	Compared to Low T	Compared to High T
Strengths	<ul style="list-style-type: none">• Lower PGM loading• Less fuel processing• Less cooling required	<ul style="list-style-type: none">• Cheaper interconnects & seals• Fewer CTE problems• Greater ability to ramp/cycle
Weaknesses	<ul style="list-style-type: none">• Longer start-up• Cycling ability less clear	<ul style="list-style-type: none">• Higher resistance & overpotentials• Fuel reforming issues

Build a community of FC, solid state materials and C-H bond catalysis scientist and technology developers.

Electrolytes for IT Fuel Cells

Not an exclusive list:

LT SOFCs

- Composite electrolytes with interfacial pathways
- Multilayer electrolytes

IT Proton Conductors

- $\text{Ba}(\text{Zr}, \text{Ce}, \text{Y})\text{O}_3$
- Solid acid fuel cells
- Indium tin pyrophosphate

Other Ionic Conductors

- HT alkaline
- HT phos acid
- LT molten carbonate

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REBELS Program Vision

A new temperature range (roughly 200-500 C) will enable new chemistries, materials, & functionalities:

1

ITFC

Efficient, reliable small power systems

- ▶ Entry markets valuing reliability, including DoD
- ▶ Low cost CHP: higher efficiency, less CO₂

2

Fuel Cell +
Additional
Functionality

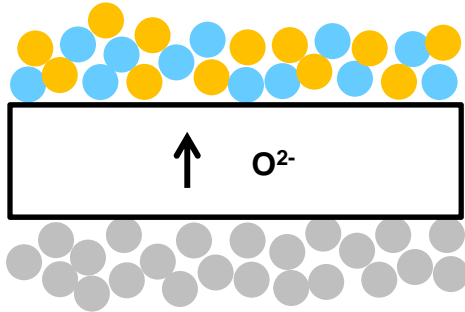
Fuel cell with integrated battery mode
for faster response to transients

3

Fuel Cell +
Additional
Functionality

Fuel cell with ability to convert natural gas
to liquid fuels

Category 1: ITFC



Fuel cannot be H₂; mostly focusing on CH₄

Final Deliverable: 100 W, 5 cell stack

ID	Category	Value
1.1	Desired operating temperature range	200-500 °C
1.2	Current density at 70% of Nernst voltage	> 200 mA/cm ²
1.3	Electrical efficiency at rated power	>50%
1.4	Startup time	< 10 minutes
1.5	Transient response	< 1 minute
1.6	Minimum stack testing time	1,000 hours
1.7	Power degradation rate	< 0.3% per 1,000 hours
1.8	Platinum group metal (PGM) total loading	< 0.1 mg PGM / cm ² electrode area

Category 1 Projects



Mixed proton, oxygen ion conducting electrolyte, single reduced T firing step



Nanostructured cell materials, low temperature reforming catalysts



Nanostructured SAFC electrode with low Pt loading, modify reformer for lower T operation



Novel electrolyte that transports oxygen in a form that enables direct reaction with fuel



Bismuth oxide/ceria bilayer electrolytes, ceramic redox-stable anodes for fuel flexibility & cycling

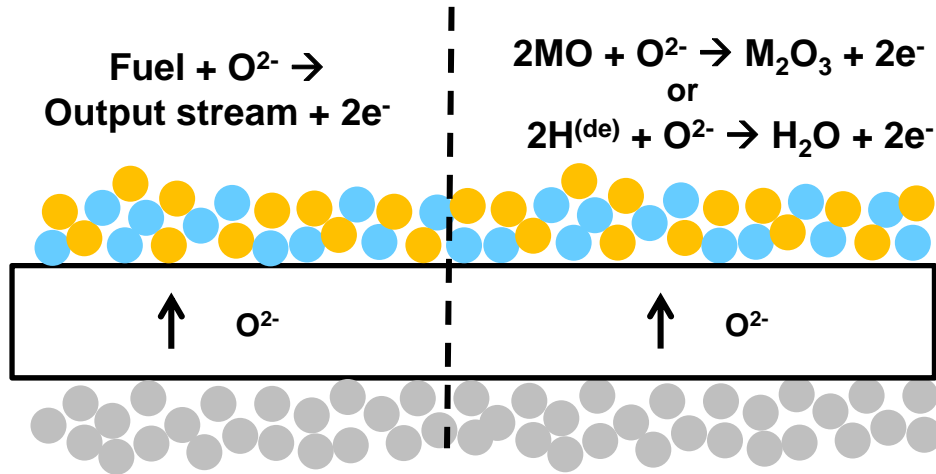


SAFC electrodes with carbon nanotubes and metal-organic framework catalysts to eliminate Pt



IT electrolyte in a metal-supported cell where the reformer is integrated with the stack

Category 2: Dynamic Response ITFC



Q. Van Overmeer, et al., Nano Lett. 12 (2012) 3756-3760

Fuel can be H_2 or a hydrocarbon

Final Deliverable: 1 cell



ID	Category	Value
2.1	Desired operating temperature	200-500 °C
2.2	Current density at 70% of Nernst voltage	> 200 mA/cm ²
2.3	Minimum stack testing time	100 hours
2.4	PGM total loading	< 0.1 mg PGM / cm ² electrode area
2.5	Battery response time	< 1 second
2.6	Time at rated power	15 minutes
2.7	Battery cycling degradation	80% of loaded capacity retained after 30 cycles
2.8	Battery mode recharge time	< 1 hour
2.9	Self-discharge rate	< 5% of loaded capacity after 12 hours
2.10	Mode switching temperature	To be specified by the applicant

Category 2 Projects



Multifunctional anode for direct hydrocarbon operation & charge storage; thin film platform

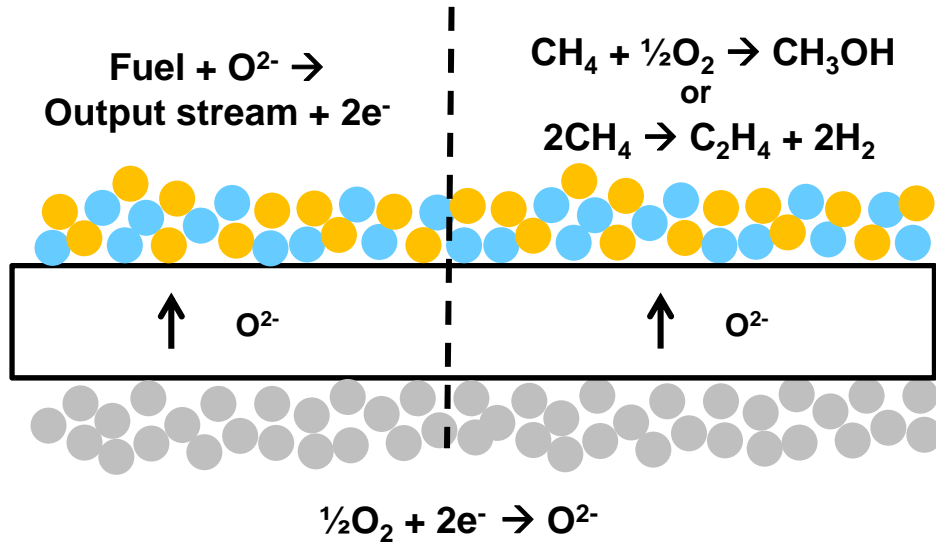


SOFC / metal-air redox battery with new solid electrolyte and Fe-based redox-active chemical bed



Metal oxide electrodes with high electronic and protonic conductivity; high charge storage capacity

Category 3: ITFC with Fuel Production



Fuel can be any hydrocarbon

Final Deliverable: 1 cell

ID	Category	Value
3.1	Desired operating temperature	200-500 °C
3.2	Current density at 70% of Nernst voltage	> 200 mA/cm ²
3.3	Continuous cell operations	> 100 hours
3.4	Minimum cell area	> 100 cm ²
3.5	Current density (during fuel production)	> 100 mA/cm ²
3.6	Cell cost per rate of product output	< \$100,000/bpd
3.7	Process intensity	> 0.1 bpd/ft ³
3.8	Product yield	> 50 %
3.9	Carbon efficiency	> 50%
3.10	Desired product(s)	To be specified by applicant
3.11	Volumetric product output per cell	To be specified by applicant (L/day)

Category 3 Projects



IT conversion of methane to ethylene enabled by a hydrogen pump



Develop IT methane-to-methanol catalysts and fabricate via reactive spray deposition technique



All thin-film ITSOFC made by mass production-enabled process with optimized electrode morphology

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ARPA-E / SECA Coordination

- ▶ Common awardees; SECA-funded work has provided the basis for several REBELS projects
- ▶ Materials are different, as well as some of the balance-of-plant considerations
- ▶ Goal is for REBELS projects to demonstrate key technical points
 - Good electrochemical performance from 200-500 C
 - Efficient fuel processing < 650 C
 - Potential for 10 year stack lifetime

Key Goal: Create new FC type technologies – life after ARPA-E

Summary

- ▶ Combination of new materials and DG needs indicated the opportunity for an ARPA-E program
- ▶ ARPA-E is excited for all 3 REBELS Categories; contracting process is currently underway
- ▶ Important to continue discussions between REBELS and SECA projects going forward